

**The University of Calgary**  
**Department of Chemical & Petroleum Engineering**

ENCH 501: Transport Processes Quiz #5

November 4, 2003

Time Allowed: 50 mins.

Name: \_\_\_\_\_

At a remote site for drilling for oil, a trailer with three rooms served as the office, the relaxation room and the dining/kitchen. The trailer is 7.5m long, 3 m wide and 2.5m high. Each of the rooms is 2.5m long. The office is located at the front end and to keep snow from blowing over the window, an 0.5m wide apron of sheet metal is wrapped around the edge (see sketch). The bottom of the trailer is covered by a skirt and this prevents flow of air over the bottom side.

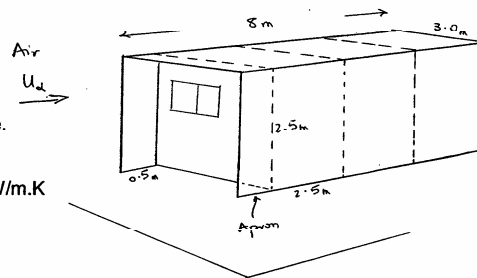
It has been suggested that on cold, windy days the office has to be heated more than the relaxation room at the other end of the trailer in order to maintain the same temperature of 18°C in each room. If the wind comes from the direction of the office at a temperature of -32°C and a velocity of 0.7m/s, estimate and compare the amounts of heat needed to be generated in the office and in the relaxation room if the sheet metal wall of the trailer (except the apron) is maintained at 18°C. That is, the apron is unheated. Also neglect heat loss from the walls perpendicular to the direction of air flow.

Show your steps and state all other assumptions.

**Hint & Data**

Assume the apron constitutes an unheated leading edge.

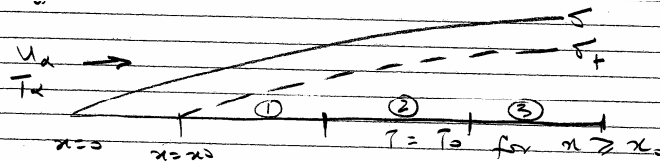
Properties of air at film conditions:  $\rho = 1.4119 \text{ kg/m}^3$ ;  
 $\mu = 0.01606 \text{ mPa}\cdot\text{s}$ ;  $C_p = 1.003 \text{ kJ/kg K}$ ;  $k = 0.02226 \text{ W/m}\cdot\text{K}$



○

Use the integral method and model this as heat loss from a flat plate of width  $2(2.5\text{ m}) + 3\text{ m} = 8\text{ m}$  and a length of  $8\text{ m}$  with  $0.5\text{ m}$  of the leading edge unheated.

That is



Interested in heat loss from wall to air between  $0.5 \leq x \leq 3.0$  and  $5.5 \leq x \leq 8.0\text{ m}$ . These are zones 1 and 3 on the plate.

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This problem has been solved in the Notes, p 113-118, by the integral method.

The heat transfer coefficient at each  $x$  is given by eq. 5.84 (p. 117 Notes)

$$h_x = 0.332 k Pr^{1/3} \left[ \frac{U_s}{\nu x} \right]^{1/2} \left[ 1 - \left( \frac{x_0}{x} \right)^{3/4} \right]^{-1/3} \quad (1)$$

Over a differential surface ( $dx \cdot W$ ) where  $W = 8\text{ m}$

$$dQ = h_x (T_0 - T_s) W dx$$

Hence

$$Q_1 = \int_{0.5}^3 h_x (T_0 - T_s) W dx \quad (2)$$

○ and  $Q_3 = \int_{5.5}^8 h_x (T_0 - T_s) W dx \quad (3)$

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- The integration of equations ② + ③ is complicated because of the function  $h_x$ . Hence a graphical method is useful. Plot  $h_x$  vs.  $x$  and estimate the averages  $h_1$  and  $h_3$  over the limits of the integral.

Then  $Q_1 = h_1 (T_0 - T_\infty) W (2.5)$

and  $Q_3 = h_3 (T_0 - T_\infty) W (2.5)$

also  $\frac{Q_1}{Q_3} = \frac{h_1}{h_3}$

→ The steps are as follow.

- Data:  $k = 0.02226 \text{ W/mK}$

$$R_f = \frac{Q_1/k}{k} = \frac{y}{x} = \frac{1003(1.606)(10^{-5})}{2.226(10^{-2})} = 0.7236$$

$$y = \frac{\mu}{\rho} = 1.1375(10^{-5}) \text{ m}^2/\text{s}$$

$$u_x = 0.7 \text{ m/s}$$

$$\therefore h_x = 1.64595 x^{-1/2} \left[ 1 - \left( \frac{x_0}{x} \right)^{3/4} \right]^{-1/3}; x_0 = 0.5 \text{ m}$$

	$x, \text{m}$	$h_x, \text{W/m}^2\text{K}$	
need	0.5	$\alpha$	
enough	0.6	4.2182	$x=0.51 \quad 7.3983$
points	1.5	1.6292	
to	3.0	1.0510	
draw a	4.5	0.8903	
smooth	5.5	0.7455	
curve.	7.0	0.6537	
	8.0	0.6084	

○ The plot of  $h_x$  vs.  $x$  is shown in fig. 1

Approximately from figure

$$h_1 = 1.8 \text{ W/m}^2\text{K}$$

$$h_3 = 0.68 \text{ W/m}^2\text{K}$$

$$\therefore Q_1 = 1.8 (18 - (-32)) (8) (2.5) = 1800 \text{ W}$$

$$Q_3 = 0.68 (50) (8) (2.5) = 680 \text{ W}$$

The ratio  $\frac{Q_1}{Q_3} = \frac{1.8}{0.68} = 2.65$

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○

K $\Sigma$  10 X 10 TO THE CENTIMETER 18 X 25 CM.  
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$h_{\pi}$   
 $\frac{Q_{\pi}}{m^2 K}$

