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## The University of Calgary Department of Chemical & Petroleum Engineering

**ENCH 501: Transport Processes Quiz #2** 

**September 21, 2004** 

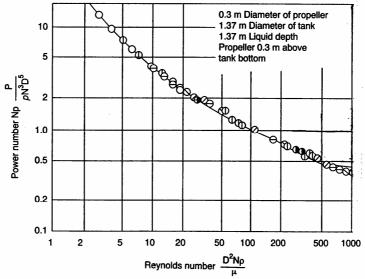
Time Allowed: 40 mins.

Name:

## Problem #1 (5 points)

In a polymerization operation, a liquid mixture ( $\rho$ = 1650 ± 60 kg/m³;  $\mu$  = 800±5 mPa s) is agitated in a tank by a propeller mixer with a diameter (**D**) of 0.5 ± 0.05 m. You are provided data for the power number (**Np**) versus Reynolds number (**Re**) for the propeller below. If the impeller rotation rate (**N**) is estimated as 15±1 rpm, what is the expected value of the power **P** of the motor required to drive the impeller? What is the error in the estimate of the power? Show all steps.

Data: (Note that the scales on the plot are log.)



## Problem #2 (5 points)

The viscosity  $\mu$  of a liquid can be determined using co-axial cylinders. The inner cylinder, radius a, is suspended on a torsion string linked to a gauge to record torque G (force on the surface times the radius). The liquid is placed in the annular space between the cylinders and the outer cylinder, radius b, is rotated at a steady rate  $\Omega$ . The viscosity is calculated from -

$$\mu = \{G / (4\pi\Omega)\} \{ 1/a^2 - 1/b^2 \}$$

If the relative error for  ${\bf a}$  is  $f_1$  and the relative error for  ${\bf b}$  is  $f_2$  (and both G and  $\Omega$  are exact), derive a relationship for the error in the viscosity. Show all steps.

If **a**=4cm, **b**=5cm and the maximum absolute error in the radii measurements is 0.01cm, what is the maximum relative error for the viscosity?

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the state of the s	no explicit equalism	
Expected ve	etue of Reynslds mu	wer (N w 5-1)
Ke	where of Reynflots run $= D^{2}NP = (0.5)$	15 (1450) 60 800 X10-3
	= 128.9	
Expected O	relue of Power M $\frac{P}{\rho N^3 D^5} \approx 0.9$	unber. Rom plot,
, Pau	per, P = 0.9 (165° = 0.725	)(0.25) <sup>3</sup> (0.5) <sup>5</sup>
To estimate e	vvov cletermine low	er a upper bound
Mus Re = (=	1.45) (14) (1590) 60 0.805	93.3
(bruesponding	8 .د ت ط	
Max Re =	(0.55)² (16) (1710)	= 173.5
Csives pooding	Np = 1.01	
; 2 Np =	$\frac{P}{PN^3D^5} = 0.9$	
ρ =	0.725 ± 0.081	W
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#2 The relationship is
$\mathcal{L} = \beta \left( \frac{1}{a^2 - \frac{1}{b^2}} \right) \text{ where } \beta = \frac{G}{4\pi 2}, \text{ a const.}$
dr = 3r da + 2r db
$d\mu = -\beta \frac{2}{3} de + \beta \frac{2}{3} db$
Given $f_1 = \frac{1}{2} \frac{dq}{dq}$ and $f_2 = \frac{1}{2} \frac{db}{dq}$
$\frac{d\mu}{dz} = \frac{1}{2} \left\{ -\frac{f_1}{f_2} + \frac{f_2}{f_2} \right\} \left( \frac{1}{a^2 - b^2} \right)$
Relative entry $dh = -2f_1b^2 + 2f_2a^2$ for viscosity, $h = -2f_1b^2 + 2f_2a^2$
Given a = 4 cm, b = 5 cm and da = db = 0.01 cm,
$\frac{1}{2} = \frac{2}{9} \left( \frac{25 \cdot 0.01}{4} + \frac{16 \cdot 0.01}{5} \right)$
where $f_1 = -\frac{0.01}{4}$ and $f_2 = \frac{0.01}{5}$ to get largest error.
2h = 0.021
j.e. eyvsy w p vi ~ 2.19_
This is about 10 times the error of measures? the radii!
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